

# ICEN Extension to SENKIN Code

Aug. 24, 2004; Aug. 22, 2007  
A. Miyoshi

This document describes the zero-dimensional internal combustion engine model used in the ICEN (Internal Combustion Engine) extension to SENKIN<sup>[1]</sup> code in Chemkin-II<sup>[2]</sup> based on Heywood.<sup>[3]</sup>

Although the model and the input parameters were intended to be compatible with the similar extension in Chemkin-3/4, the calculation results are not assured to be the same as them.

## 1. Nomenclature

The symbols and abbreviation used in this document are listed below.

$a$	Crank radius	$A$	Surface area
$A_{ch}$	Cylinder head surface area	$A_p$	Piston crown surface area
$B$	Cylinder bore	$c_p$	Isobaric specific heat capacity
$C_{p,m}$	Isobaric molar heat capacity	$h_c$	Heat-transfer coefficient
$k$	Thermal conductivity	$K$	Compression ratio
$l$	Connecting rod length	$L$	Piston stroke
$M_{air}$	Molar mass of air	$N$	Crankshaft rotational speed ( $= \omega / 2\pi$ )
$p$	Pressure	$Q$	Heat
$R$	connecting rod length / crank radius	$R_{gas}$	Molar gas constant
$s$	Crank axis to piston pin distance	$\hat{S}_p$	Mean piston speed
$t$	Time	$T$	Temperature
$T_w$	Cylinder wall temperature	$V_c$	Clearance volume
$V_d$	Displaced cylinder volume	$\theta$	Crank angle ATDC (after TDC)
$\delta_h$	Thickness of thermal boundary layer	$\rho$	Density
$\mu$	Viscosity	$Nu$	Nusselt number ( $= h_c B / k$ )
$\omega$	Crankshaft angular velocity ( $= 2\pi N$ )	$Re$	Reynolds number ( $= \rho \hat{S}_p B / \mu$ )
BDC	Bottom dead center		
$Pr$	Prandtl number ( $= c_p \mu / k$ )		
TDC	Top dead center		

## 2. Piston-Crank Mechanism

From a geometric consideration, as depicted in Fig. 1, the distance,  $s$ , between the crank axis and piston pin axis can be written as,

$$s = a \cos \theta + \sqrt{l^2 - a^2 \sin^2 \theta} \quad (1)$$

Since the distance  $s$  at the TDC is  $s_{TDC} = a + l$ , the cylinder volume is,

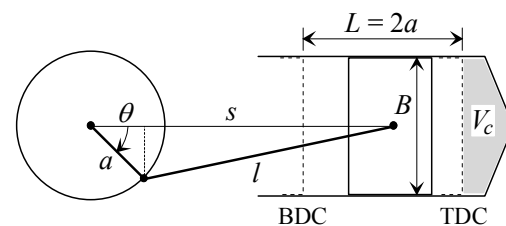


Fig. 1 Schematics of the Piston-Crank Mechanism

<sup>[1]</sup> A. E. Lutz, R. J. Kee, and J. A. Miller, SENKIN: A Fortran Program for Predicting Homogeneous Gas Phase Chemical Kinetics With Sensitivity Analysis, SAND87-8248-UC-401, Sandia National Laboratories, 1995.

<sup>[2]</sup> R. J. Kee, F. M. Rupley, and J. A. Miller, Chemkin-II: A Fortran Chemical Kinetics Package for the Analysis of Gas-Phase Chemical Kinetics, SAND89-8009B-UC-706, Sandia National Laboratories, 1995.

<sup>[3]</sup> J. B. Heywood, Internal Combustion Engine Fundamentals, McGraw-Hill, New York, 1988.

$$V = \frac{\pi B^2}{4} (s_{\text{TDC}} - s) + V_c \quad (2)$$

By using the ratio of connecting rod length to crank radius,

$$R = \frac{l}{a} \quad (3)$$

and the compression ratio,

$$K = \frac{V_d + V_c}{V_c} = \frac{\pi B^2 a}{2V_c} + 1 \quad (4)$$

eq. (2) can be rewritten as,

$$\frac{V}{V_c} = \frac{K-1}{2} \left( 1 + R - \cos \theta - \sqrt{R^2 - \sin^2 \theta} \right) + 1 \quad (5)$$

For a constant angular velocity, the time variation is described with,

$$\theta = \theta_0 + \omega t \quad (6)$$

where  $\theta_0$  is the crank angle at  $t = 0$ . Differentiation of eq. (5) with respect to  $\theta$  gives,

$$\frac{1}{V_c} \frac{dV}{d\theta} = \frac{K-1}{2} \sin \theta \left( 1 + \frac{\cos \theta}{\sqrt{R^2 - \sin^2 \theta}} \right) \quad (7)$$

The time derivative of the volume is given by,

$$\frac{dV}{dt} = \omega \frac{dV}{d\theta} \quad (8)$$

Similarly, the cylinder surface area is given by,

$$A = A_{\text{ch}} + A_p + \frac{2V_c(K-1)}{B} \left( 1 + R - \cos \theta - \sqrt{R^2 - \sin^2 \theta} \right) \quad (9)$$

For flat-topped piston and cylinder,

$$A_p = \frac{\pi B^2}{4} \quad (10)$$

$$A_{\text{ch}} = \frac{\pi B^2}{4} + \frac{4V_c}{B} \quad (11)$$

The mean piston speed is defined as,

$$\hat{S}_p = 2LN = \frac{8V_c(K-1)}{\pi B^2} N \quad (12)$$

### 3. Heat Transfer

For a forced-convection condition, the rate of heat-transfer is described by,

$$\frac{dQ}{dt} = h_c A (T - T_w) \quad (1)$$

The heat-transfer coefficient  $h_c$  is related to the thermal conductivity  $k$  and the thickness of the thermal boundary layer  $\delta_h$  by a simple boundary layer model,

$$h_c = \frac{k}{\delta_h} \quad (2)$$

Thus the main problem of the forced-convection heat-transfer is in the estimation of  $\delta_h$  or the Nusselt dimensionless number  $Nu$ ,

$$Nu = \frac{B}{\delta_h} = \frac{h_c B}{k} \quad (3)$$

Note that in this document, the *characteristic length* in a dimensionless number is taken to be the cylinder bore  $B$ . In many empirical correlations,  $Nu$  is written by Reynolds and Prandtl numbers,  $Re$  and  $Pr$ , respectively, as,

$$Nu = a Re^m Pr^n \quad (4)$$

The Reynolds and Prandtl numbers are defined as,

$$Re = \frac{\rho \hat{S}_p B}{\mu} \quad (5)$$

$$Pr = \frac{c_p \mu}{k} \quad (6)$$

By assuming that the gas property is dominated by that of air,  $\rho$ ,  $k$ ,  $\mu$ , and  $c_p$  are approximated as,

$$k \approx k(\text{air}) = 3.50 \times 10^{-4} T^{0.764} [\text{J m}^{-1} \text{s}^{-1} \text{K}^{-1}] \quad (7)$$

$$= 35.0 T^{0.764} [\text{erg cm}^{-1} \text{s}^{-1} \text{K}^{-1}] \quad (7')$$

$$\mu \approx \mu(\text{air}) = 4.41 \times 10^{-7} T^{0.664} [\text{kg m}^{-1} \text{s}^{-1} = \text{Pa s} = \text{N s m}^{-2}] \quad (8)$$

$$= 4.41 \times 10^{-6} T^{0.664} [\text{g cm}^{-1} \text{s}^{-1} = \text{dyn s cm}^{-2}] \quad (8')$$

Widely used Woschni's correlation assumes that  $a = 0.035$  and  $n = 0$  in eq. (4),

$$Nu = 0.035 Re^m \quad (9)$$

In many cases, the exponent  $m$  is chosen to be 0.8.